# **AR ${AR}: Install Heat Exchanger to Recover Heat from Exhaust Gas**

**Recommended Action**

Recover exhaust heat from the thermal oxidizer and use this recovered heat to preheat the air for the drying ovens by applying a heat exchanger.

**Summary of Estimated Savings and Implementation Costs**

|  |  |
| --- | --- |
| Annual Cost Savings | ${ACS} |
| Implementation Cost | ${IC} |
| Payback Period | ${PB} |
| Annual Natural Gas Savings | ${NGS} MMBtu |
| Annual Electricity Savings | ${ES} kWh |
| Annual Demand Savings | ${DS} kWh |
| ARC Number | 2.2442.2 |

**Current Practice and Observations**

The furnace is exhausting heat to the atmosphere at about ${TI}oF with a volume of ${CFM} CFM. This exhaust heat can be recovered for use in the plant.

**Anticipated Savings**

The potential Natural Gas Savings, NGS, and cost savings, CS, can be estimated as follows:

NGS =

CS = NGS × Unit cost of gas,

where

= Density of exhaust gas (at ${TI}oF); ${RHO} lb/ft3

Cp = Specific heat of exhaust gas[[1]](#footnote-1) (at ${TI}oF); ${CP} Btu/lb°F

CFM = Total exhaust flow rate of furnaces; ${CFM} ft3/min

C1 = Conversion constant; 60 min/h

Ti = Temperature of exhaust air at the entry of heat exchanger; ${TI}°F

η = Efficiency of air-air heat exchanger; conservatively ${ETA}% (depends on design)[[2]](#footnote-2)

To = Temperature of exhaust air at the exit of heat exchanger; ${TO}°F

OH = Oxidizer operating hours; ${OH} hr/yr

C2 = Conversion constant; 1,000,000 Btu/MMBtu

Using the parameters discussed above, the natural gas savings (NGS) and cost savings (NGCS) can be calculated as follows:

NGS = #NGSEqn

= ${NGS} MMBtu/yr.

CS = ${NGS} MMBtu/yr × ${NGC}/MMBtu

= ${CS}/yr.

There will be an increase in electrical energy as a fan will be required to move the hot air through the heat exchanger and into the oven inlets. The associated cost is as follows:

HP = Fan Horsepower; ${HP} HP

C3 = Conversion constant; 0.746 kW/HP

EC = Energy Cost; ${EC}/kWh

DC = Demand Cost; ${DC}/kWh

PFC = Potential Fan Cost;

= -(HP × C3) × (OH × EC + 12 × DC)

= -(${HP} HP × 0.746) × (${OH} hr/yr × ${EC}/kWh + 12 × ${DC}/kW)

= ${ES} kWh/yr × ${EC}/kWh + ${DS} kW/yr × ${DC}/kW

= ${ECS}/yr + ${DCS}/yr

= ${PFC}/yr

The Annual Cost savings; ACS; is equal to:

ACS = CS + PFC;

= ${CS} + ${PFC}

= ${ACS}/yr

**Implementation Cost**

The implementation cost is associated with installing the heat exchanger, fan, and ducting to the existing oven inlets. This is estimated at ${IC}.

**The annual natural gas savings for this AR will be ${NGS} MMBtu. The estimated annual cost savings is likely to be ${ACS} and, with ${IC} in implementation costs, the payback period will be ${PB}.**

**Implementation Cost References**

The below links are for implementation cost references. We do not endorse/recommend these brands or products. Furthermore, these products may or may not be suitable for the application. The client should contact a vendor(s) to conduct a detailed study of the process, in

order to determine the best product for the recommended application.

* A Guide to Heat Exchangers for Industrial Heat Recovery- New York State Energy Research and Development Authority cites the payback period for heat recovery - specifically, economizers and waste heat from boilers- between 2 and 3 years.
* Boiler Economizer Systems - Presented by: Hayward Burton, H.V. Burton Co. cites the average payback period for economizers and other heat recovery as 3 years.
* Willems, Daniel. “Advanced System Controls and Energy Savings for Industrial Boilers.” ASME 2006 Citrus Engineering Conference, 2006, https://doi.org/10.1115/cec2006-5202. Cites the payback period as 2 years for heat recovery projects.

1. Density and specific heat of exhaust gas is approximated to the properties of air. [↑](#footnote-ref-1)
2. Sunden, B. "Heat exchangers and heat recovery processes in gas turbine systems." *Modern Gas Turbine Systems*. Woodhead Publishing, 2013. 229. Cited as 80-93% [↑](#footnote-ref-2)